

The Concept of Chemical Similarity for Optimization and Design of Gas-Solid Processes

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- Example:
 - **The Importance of Radicals**
 - From the Single Particle to the Pilot-scale

Principal Problems in Chemical Engineering

- **Reactor/Process Design?**
- **Operating Conditions?**

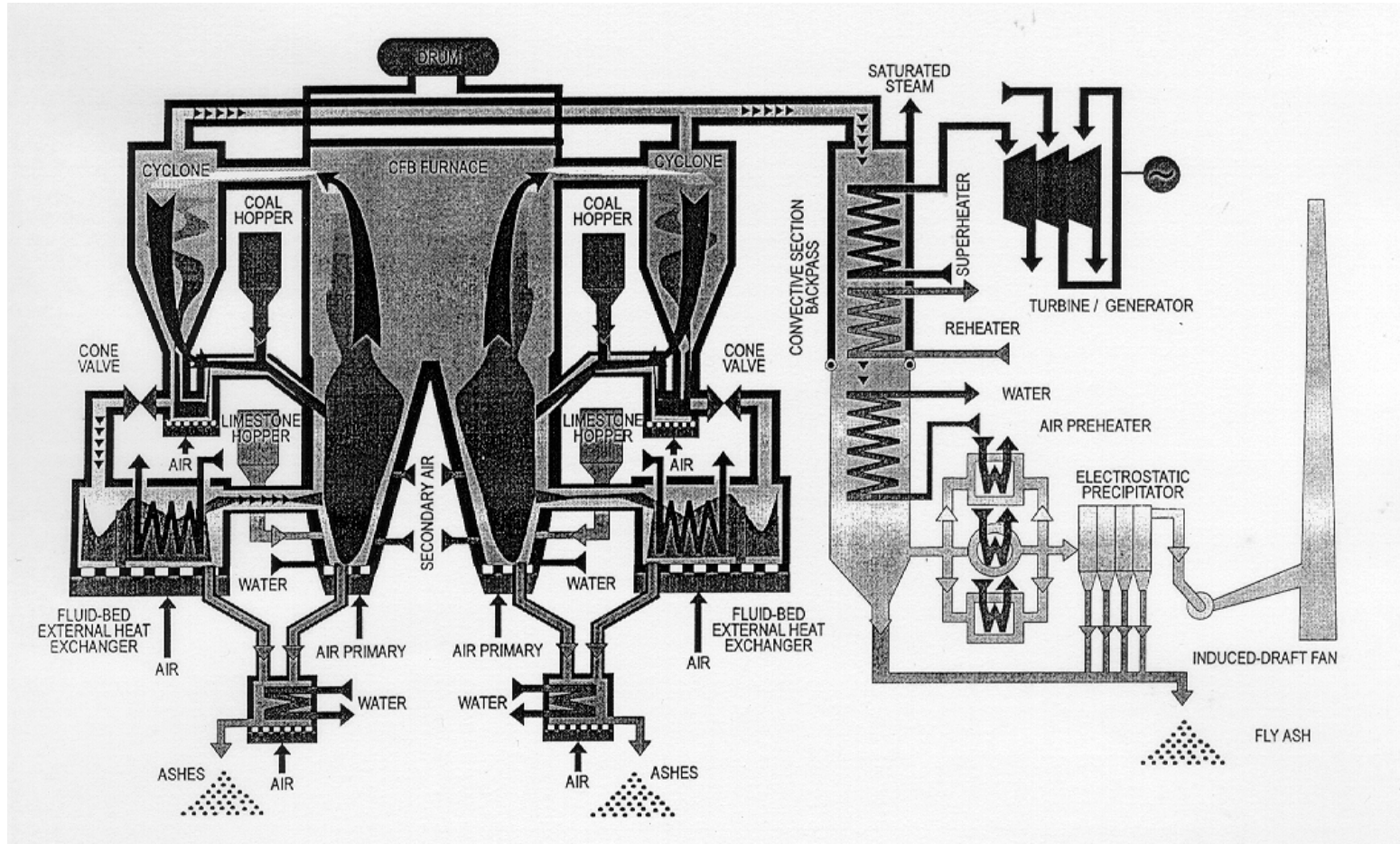
to achieve:

- **High Productivity!**
- **High Quality!**

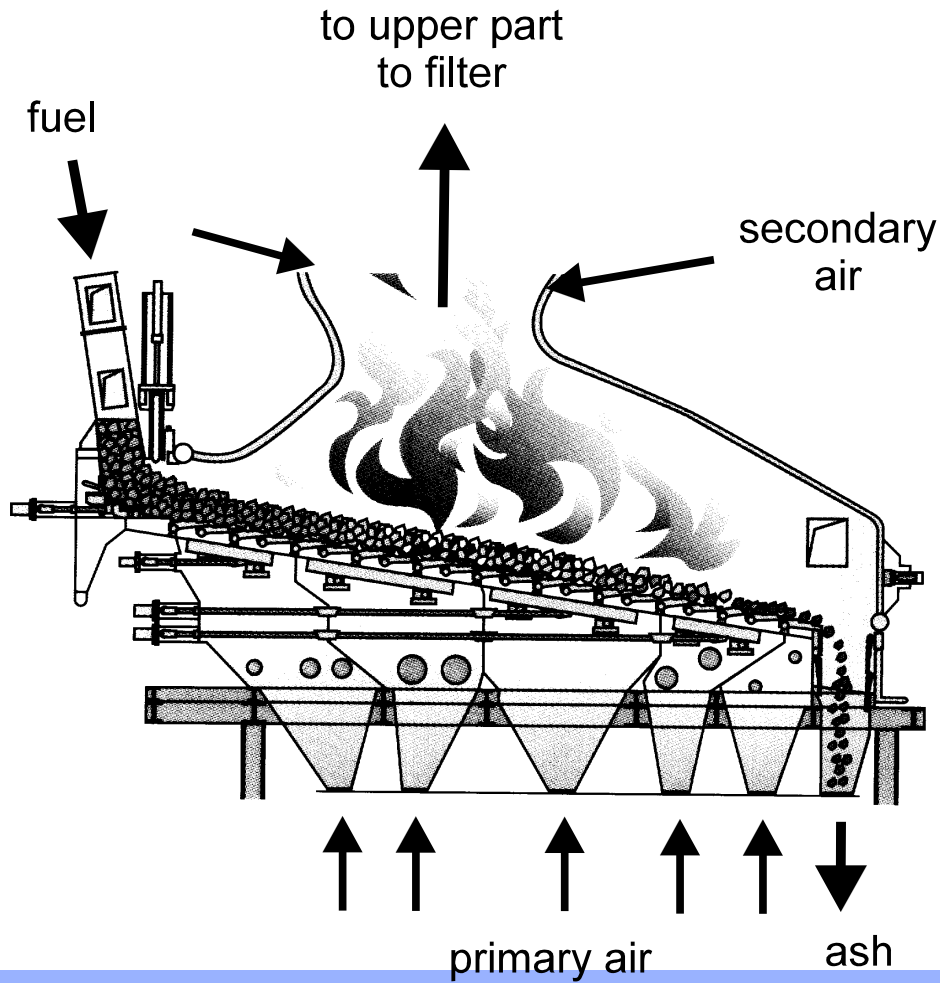
at

- **Clean Environment**
- **Low Costs**
- **Short Time**

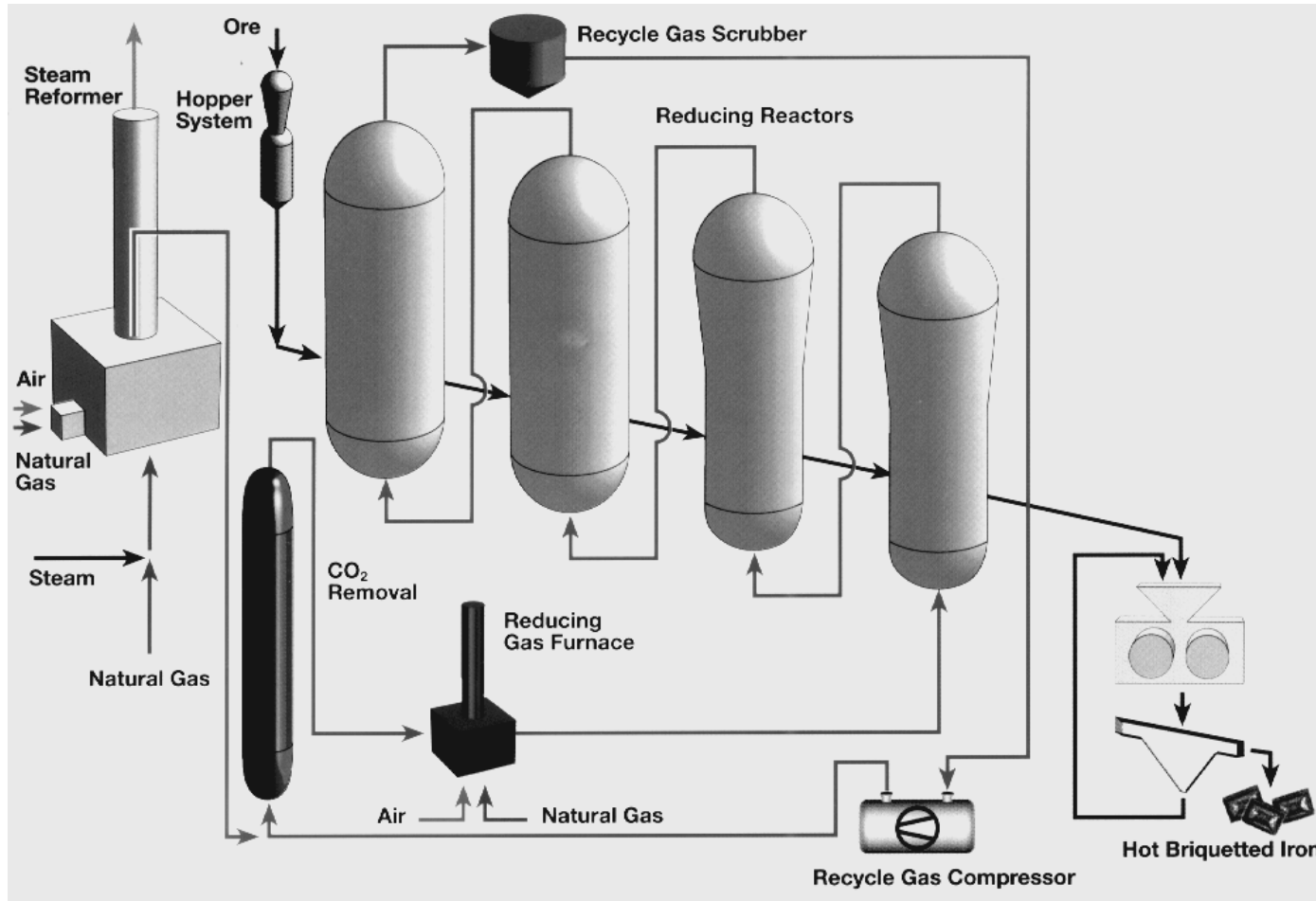
Industrial-scale Processes - Fluidized Bed Combustion



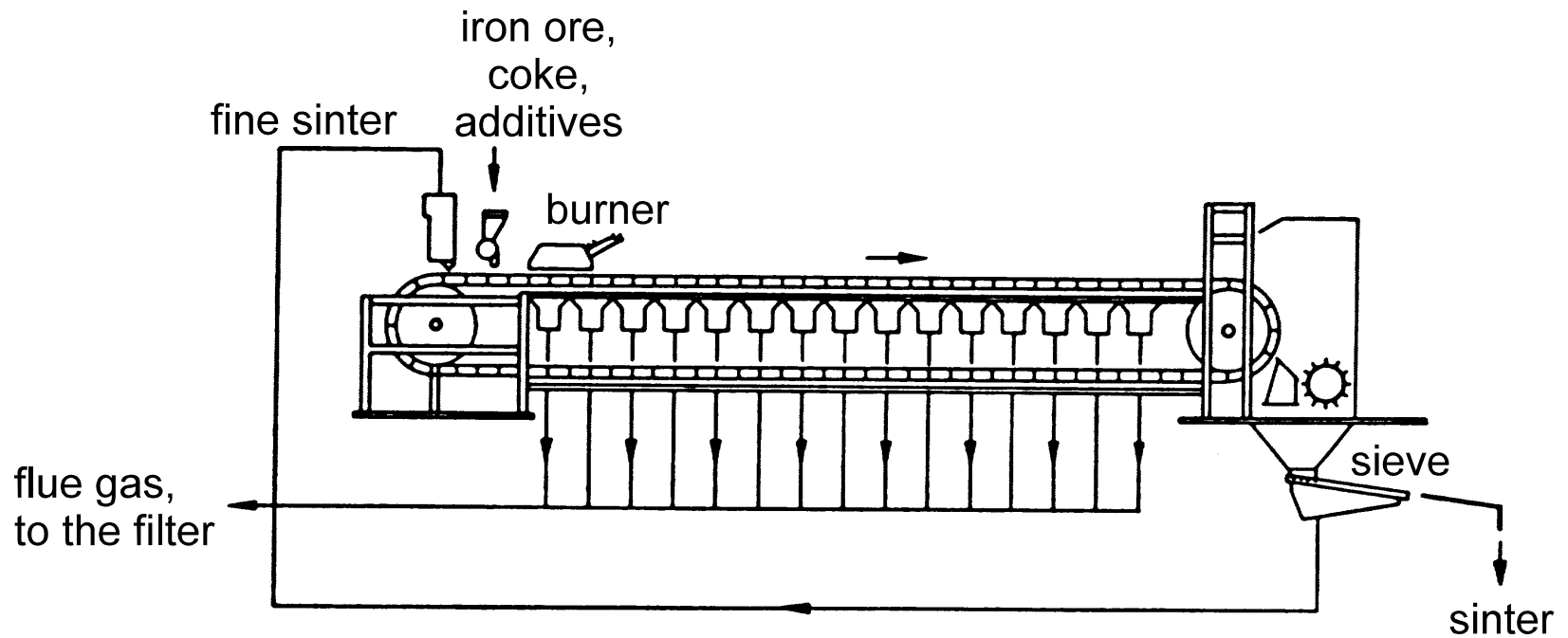
Industrial-scale Processes - Grate Combustion



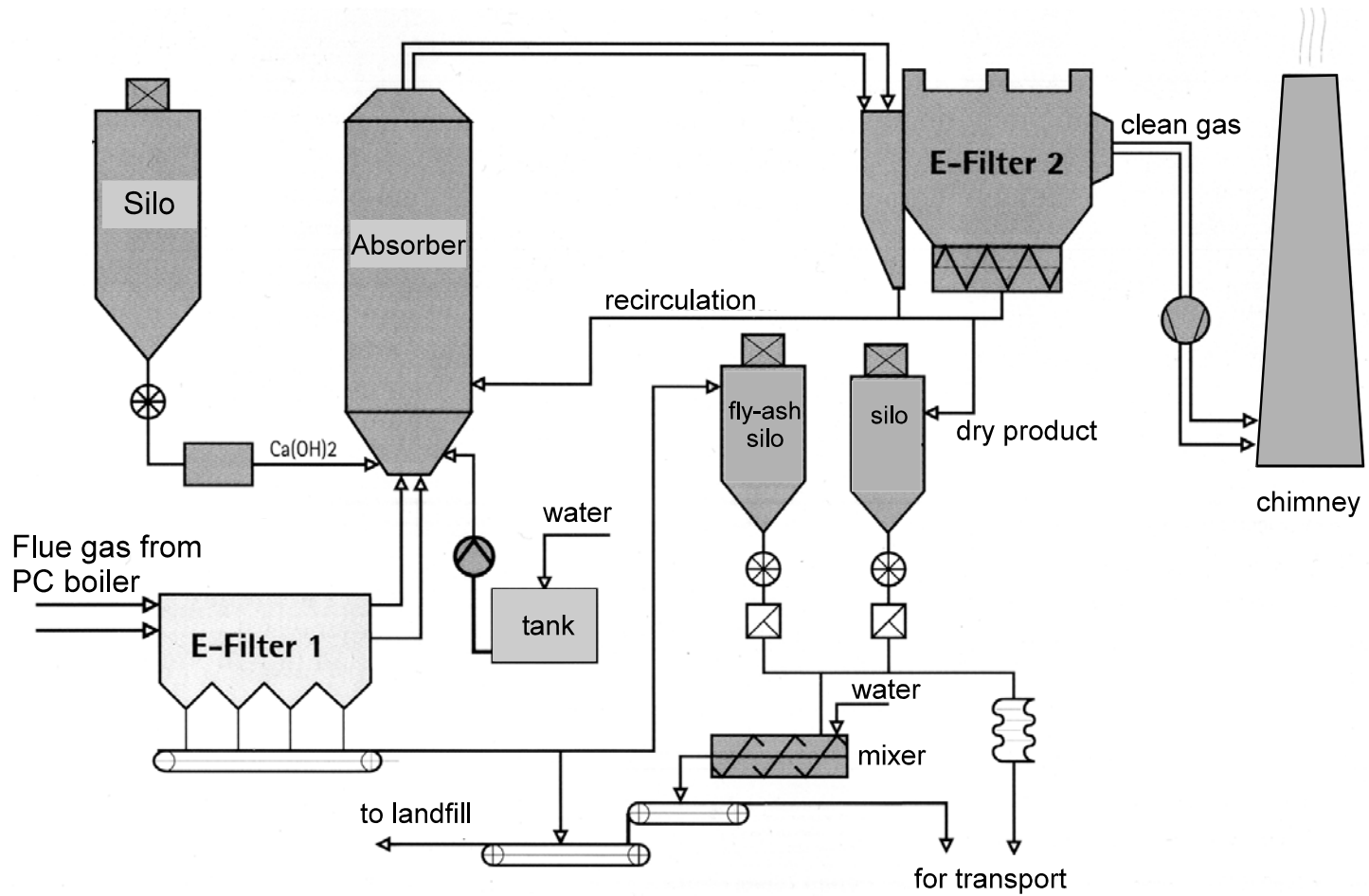
Industrial-scale Processes - Iron Ore Reduction



Industrial-scale Processes - Iron Ore Sintering



Industrial-scale Processes - Flue Gas Desulfurization



Industrial-scale Processes - Conditions

| | Combustion | | | Iron Ore Reduction | Sinter Process | De- sulfurization |
|------------------------------|----------------------|--|-------------------------------------|--------------------------------------|---|---|
| techn. | fixed | fluidized | entrained | fluidized | fixed | fluidized |
| gaseous reactants | O ₂ (air) | O ₂ (air) | O ₂ (air) | H ₂ , CO, CH ₄ | O ₂ (air) | SO ₂ , CO ₂ , HCl |
| solids' temp. | 400-1000 | 600-950 | 900-1700 | 600-900 | 800-1400 | 60-150 |
| pressure | atmos | 1-17 | atmos | ~11 | atmos | atmos |
| sup. gas velocity | 1-4 | 1-2.5 3-8 | 5-10 | ~1 | 1 (cold) | 1-5 |
| solid reactants | biomass, waste | coals, biomass, waste, sludge | coals, co- comb. with biomass | iron ore | cokes, alternative fuels, met. waste | Ca(OH) ₂ |

Industrial-scale Processes - Conditions

| | Combustion | | | Iron Ore Reduction | Sinter Process | De- sulfurization |
|-----------------------------------|----------------------|----------------------------------|---|-----------------------------------|----------------------------------|---|
| tech- nology | fixed | fluidized | entrained | fluidized | fixed | fluidized |
| particle size | 10-100 | 1-30 0.5-10 | 0.010-0.100 | 0.05-6 | 0.2-5 (cokes) | 0.001-0.01 |
| heating rates | low | medium- high | very high | medium- high | high | low |
| lab- scale methods | - TGA - fixed bed | -fluid. bed (bubb., circ.) | -entrained -burners -grid heaters -matrix react. | - fluidized bed - fixed bed | -fixed bed - fluidized bed | - TGA - fluidized bed (circulating) |

Laboratory-Scale Units

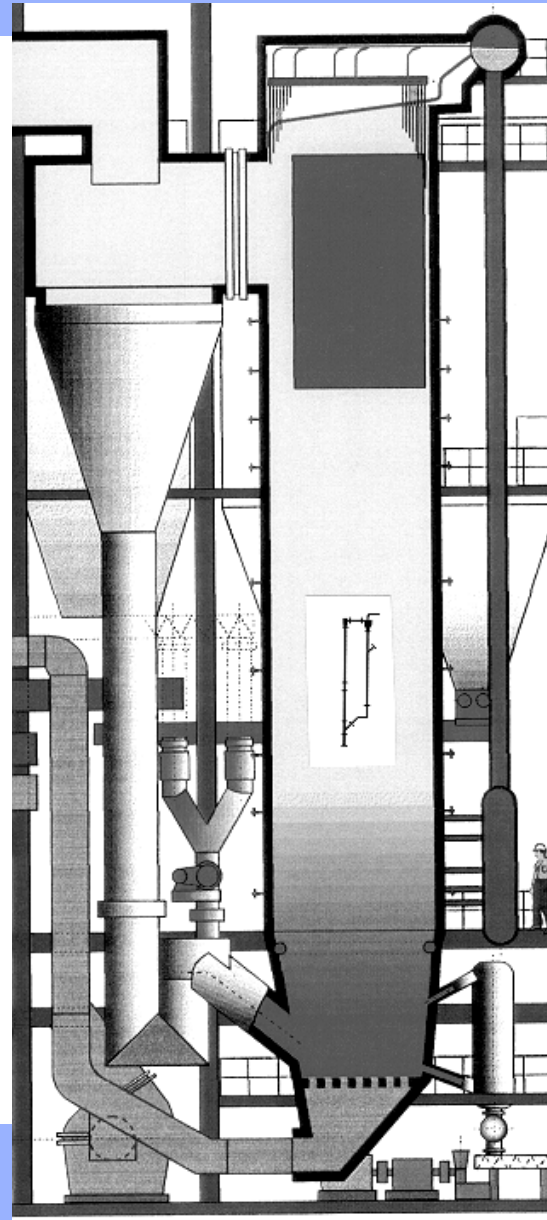
ADVANTAGES:

- inexpensive
- low operation costs
- high availability
- design changes -
quickly & low cost
- operating conditions -
broad range
- good instrumentation

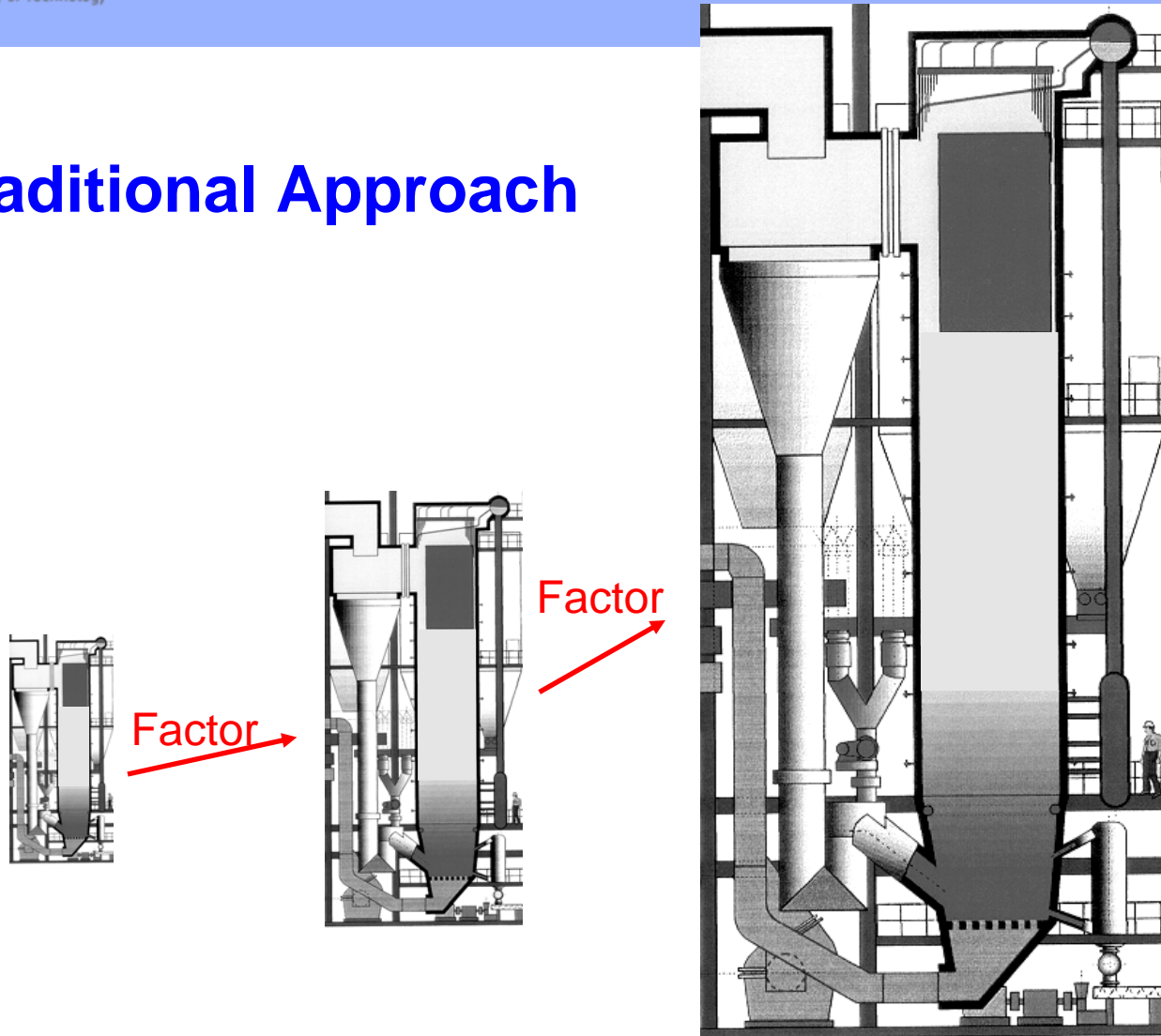
DISADVANTAGES:

- **uncertainty to transfer
results to industrial-
scale units**

Comparison between Laboratory-scale & Industrial-scale Units



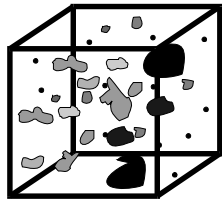
The Traditional Approach



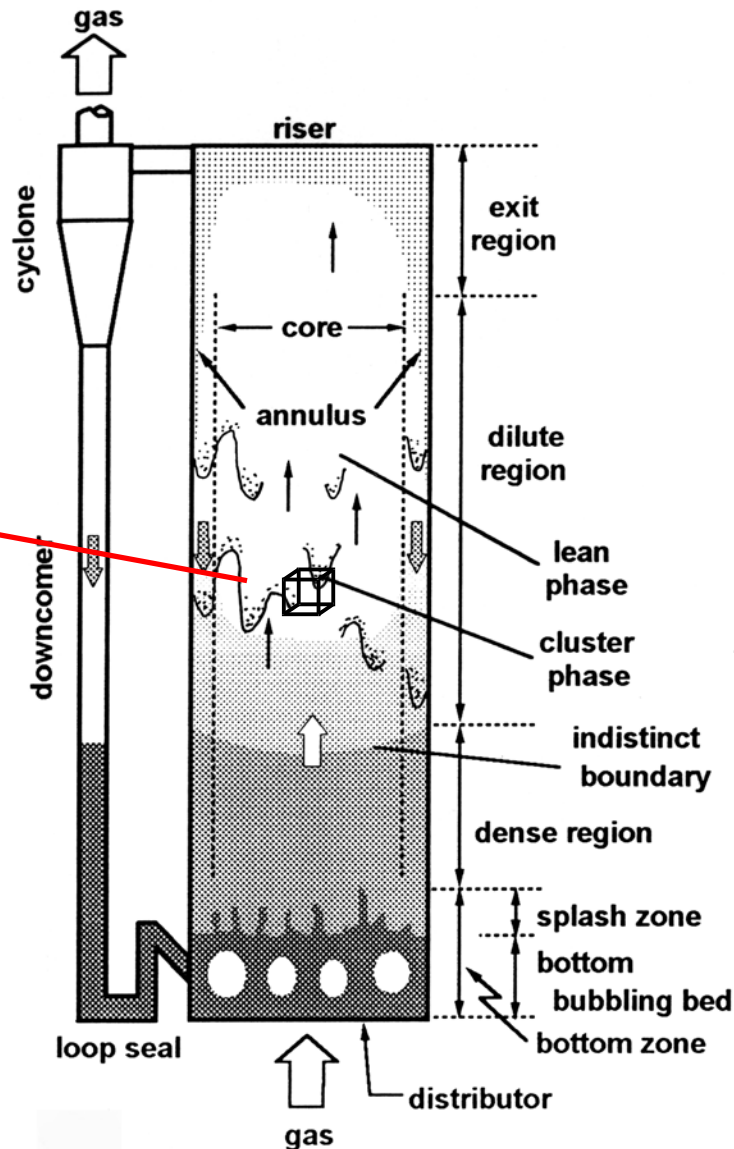
The Traditional Approach

| reactor/system | characterizing dimensionless groups |
|---|--|
| flow tube | $Re, Eu, L/d$ |
| + particles in flow tube (two phase flow) | + $Re_p, Fr_p, Ar, \rho/\rho_p, L/d_p, \Psi, \phi_s$ |
| + heat transfer to particles | + Nu_p, Pr |
| + mass transfer to particles | + Sh, Sc |
| + non-isothermal particles | + Bi_h |
| + concentration profiles in particles | + Bi_m |
| + chemical reactions in flow tube | + DaI |
| + mixing effects | + $Bo (Pe)$ |
| + chemical reactions inside particles | + $DaII, \phi$ |

The Concept of Chemical Similarity



Finite Volume



Chemical Similarity Rules - homogeneous systems

A Pure Homogeneous Reaction System:

At a given time, it is:

- gas temperature (T_g)
- total pressure (P)
- species concentration ($C_1, \dots, C_i, \dots, C_z$)

$$r_{hom,i} = \frac{dN_i}{dt} \cdot \frac{1}{V_R} = f_{hom,i}(T_g, P, C_1, \dots, C_i, \dots, C_z)$$

Chemical Similarity Rules - gas-solid systems

A Gas - Solid Reaction System:

in addition:

- the particle temperature (T_p)
- the gas temperature inside the pores of the particle ($T_{g,pore}$)
- the pressure inside the particle (P_p)
- the species' concentrations inside the pores of the particle ($C_{1,p}, \dots, C_{i,p}, \dots, C_{z,p}$)
- the species' concentrations at the surface of the particle ($C_{1,s}, \dots, C_{i,s}, \dots, C_{z,s}$)
- the physical properties of the solid reactant such as external/internal surface area (A_s), pore structure ($X_{p,pores}$)
- the chemical composition of the solid reactant ($X_{p,chem}$)

$$r_{het,i,A} = \frac{dN_i}{dt} \cdot \frac{1}{m_{p,A}} = f_{het,A}(T_{p,A}, T_{g,pore}, P_{p,A}, P, A_{s,A}, X_{p,pores,A}, X_{p,chem,A}, C_{1,p,A}, \dots, C_{i,p,A}, \dots, C_{z,p,A}, C_{1,s,A}, \dots, C_{i,s,A}, \dots, C_{z,s,A})$$

Chemical Similarity Rules - Consequences/Problems

- the actual fuel or solid reactant of the industrial-scale process has to be used in the laboratory-scale
- artificial fuels or solid reactants with well-known compositions can be used as model fuels for the calibration of test units

But even if the same solid reactant is used in laboratory-scale tests different results can be obtained ...

- ⇒ different heating rates of the solid reactant
- ⇒ memory effects and fluctuations of conditions
- ⇒ particle - particle interactions

Chemical Similarity - Conclusions

- It is often not possible to fulfill ***all*** those very stringent similarity rules to derive chemical kinetics in laboratory-scale units.
- However, ***useful information*** can be obtained, if the researcher is ***aware of the problems*** in designing laboratory-scale tests. He or she will know the ***limitations*** and will use the ***obtained results*** in a ***proper way*** depending on the ***aim of the work***.

Thank you for your attention!

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